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# **Recovery of Toxic Metal Ions from Washing Effluent Containing Excess Aminopolycarboxylate Chelant in Solution**

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## **Abstract**

Aminopolycarboxylate chelants (APCs) are extremely useful for a variety of industrial applications, including the treatment of toxic metal-contaminated solid waste materials. Because non-toxic matrix elements compete with toxic metals for the binding sites of APCs, an excess of chelant is commonly added to ensure the adequate sequestration of toxic metal contaminants during waste treatment operations. The major environmental impacts of APCs are related to their ability to solubilize toxic heavy metals. If APCs are not sufficiently eliminated from the effluent, the aqueous transport of metals can occur through the introduction of APCs into the natural environment, increasing the magnitude of associated toxicity. Although several techniques that focus primarily on the degradation of APCs at the pre-release step have been proposed, methods that recycle not only the processed water, but also provide the option to recover and reuse the metals, might be economically feasible, considering the high costs involved due to the chelants used in metal ion sequestration. In this paper, we propose a separation process for the recovery of metals from effluents that contain an excess of APCs. Additionally, the option of recycling the processed water using a solid phase extraction (SPE) system with an ion-selective immobilized macrocyclic material, commonly known as a molecular recognition technology (MRT) gel, is presented. Simulated effluents containing As(V), Cd(II), Cr(III), Pb(II) or Se(IV) in the presence of APCs at molar ratios of 1:50 in H<sub>2</sub>O were studied with a flow rate of 0.2 mL min<sup>-1</sup>. The ‘captured’ ions in the SPE system were quantitatively eluted with HNO<sub>3</sub>. The effects of solution pH, metal-chelant stability constants and matrix elements were assessed. Better separation performance for the metals was achieved with the MRT-SPE compared to other SPE materials. Our proposed technique offers the advantage of a non-destructive separation of both metal ions and chelants compared to conventional treatment options for such effluents.

## **Keywords**

Metal recovery; aminopolycarboxylate chelants; non-destructive separation; solid phase extraction; molecular recognition technology gel; washing effluents; wastewater treatment.

## 1.0 Introduction

Aminopolycarboxylate chelants (APCs) are used in a variety of industrial processes, for example, metal plating or finishing, textile and paper manufacturing, industrial cleaning, and water softening (Conway et al., 1999; Nowack and VanBriesen, 2005). They have also been applied to the remediation of toxic metal-contaminated solid waste materials (Raghavan et al., 1991; Grasso, 1993; Abumaizar and Khan, 1996; Peters, 1999; Roundhill, 2001; Chang et al., 2007). Because ethylenediaminetetraacetic acid (EDTA) forms strong water-soluble chelant complexes with most toxic metals (Egli, 2001; Nowack and VanBriesen, 2005; Leštan et al., 2008), it has been utilized most often among the APCs.

Although APCs have received widespread acclaim for their excellent metal-binding capacities, the pre- and post-toxicities of APCs and related environmental consequences evoke many concerns (Rahman et al., 2011c). When APCs are released into aquatic environments, they may induce the remobilization of metal ions from soils and sediments into the water phase (Means et al., 1980; Nowack and VanBriesen, 2005), therefore extending the residence time of the metals. When APCs enter the environment, the exposure effects from APCs are likely to persist for a long time because of their poor photo-, chemo- and biodegradability (Means et al., 1980; Kari and Giger, 1995; Egli, 2001; Nowack, 2002; Nörtemann, 2005). Additionally, in most cases, the toxicity threshold values of APCs increase with metal complexation (Sillanpää and Oikari, 1996; Sorvari and Sillanpää, 1996; Sillanpää, 2005). APCs can also contribute to eutrophication by increasing the total nitrogen content and phosphate solubility in interstitial waters (Horstmann and Gelpke, 1991; Erel and Morgan, 1992; Hering and Morel, 2002). Legislative agencies have become more concerned about eco-environmental consequences due to the increasing use of APCs, and increasingly stringent environmental regulations have been imposed (Grundler et al., 2005; van Ginkel and Geerts, 2005). Therefore, the treatment of industrial effluents and metal-contaminated

wastewaters from other sources containing APCs is a prerequisite before they can be safely discharged. The characteristics and concentrations of both the added chelant and metals in the source solutions are important factors to consider when determining methods of treatment (Juang et al., 1999). A degradation treatment of APCs in solution is considered when the concentration falls below 1 mM (Juang and Wang, 2000b), and several methods have been proposed to obliterate and reduce the concentration of chelant in discharge waters (Krapfenbauer and Getoff, 1999; Muñoz and von Sonntag, 2000; Bucheli-Witschel and Egli, 2001; Rämö and Sillanpää, 2001; Sillanpää and Pirkanniemi, 2001; Pirkanniemi et al., 2007). However, the recovery and reuse of APCs and metals become the main concern for concentrations above 5 mM in solution (Juang and Wang, 2000a) because the cost of chelants is a critical issue surrounding their use in metal ion sequestration (Kim and Ong, 1999; Lim et al., 2005; Leštan et al., 2008). An electrochemical reduction treatment followed by membrane separation (Juang and Wang, 2000a; Arévalo et al., 2002), a precipitation treatment with zero-valent metals (Lee and Marshall, 2002) or the addition of suitable reagents (e.g., NaOH, Ca(OH)<sub>2</sub>, Na<sub>2</sub>S, FeSO<sub>4</sub>, FeCl<sub>3</sub>, NaH<sub>2</sub>PO<sub>4</sub>, Na<sub>2</sub>HPO<sub>4</sub>, or diethyldithiocarbamate) (Tünay and Kabdasli, 1994; Chang, 1995; Steele and Pichtel, 1998; Hong et al., 1999; Kim and Ong, 1999; Xie and Marshall, 2001; Di Palma et al., 2003; Lim et al., 2005) are potential techniques proposed for the recovery of metal ions from metal-chelant solutions. Operational problems, such as membrane fouling, membrane degradation, considerable costs or the inherent stability of metal-chelant complexes in solution, are some drawbacks of the proposed separation techniques (Kim and Ong, 1999; Di Palma et al., 2003; Lim et al., 2005). Most of the proposed separation techniques are also based on equimolar solutions of metals and APCs (Chang, 1995; Kim and Ong, 1999; Juang and Wang, 2000a), while washing effluents from metal-contaminated solid-waste treatment processes are often characterized by a large excess of free APCs in solution or APCs that are combined with

other competitive ions in the waste (Di Palma et al., 2003; Leštan et al., 2008). A technique that ensures the effortless selective separation of metal ions and recycling of processed water, including APCs, may therefore be economically beneficial (Lim et al., 2005; Leštan et al., 2008).

The separation of metal ions from complex aqueous matrices using solid sorbent materials, a process known as solid phase extraction (SPE), has increased in popularity in recent years. SPE possesses the capability to interact with a variety of metal ions, and it has also been shown to interact with fairly specific selectivity to one particular ion of interest (Nickson et al., 1995; Hosten and Welz, 1999; Ghaedi et al., 2006; 2007; 2008; Rahman et al., 2011a; 2011b). SPE systems have not been used extensively for the separation of metal ions from wastewaters containing APCs because APCs compete with SPE materials for complexation of metal ions, which causes a remarkable decrease in the extraction efficiency (Hasegawa et al., 2010; 2011).

In this work, we propose a technique for the separation of toxic metal ions from synthetic effluents containing a large excess of APCs in solution. An ion-selective SPE system with immobilized macrocyclic material, commonly known as molecular recognition technology (MRT) gel (Bradshaw et al., 1988; Izatt et al., 1994; Izatt et al., 1995), was used to achieve a quantitative recovery of metal ions. Unique features of the proposed separation process include the nondestructive recovery of toxic metal ions from the excess APC-containing aqueous matrix and the one-step clean-up of the effluent with an option for recycling the processed water.

## **2.0 Material and Methods**

### ***2.1 Instrumentation***

An inductively coupled plasma optical emission spectrometer (ICP-OES) (iCAP 6300, Thermo Fisher Scientific Inc., MA, USA), composed of an EMT duo quartz torch, glass

spray chamber and concentric glass nebulizer, was used for the chemical analysis of metals. The operating conditions for the ICP-OES were as follows: the RF power at the torch was 1.15 kW, the plasma gas flow was 12 L min<sup>-1</sup>, the auxiliary gas flow was 1 L min<sup>-1</sup>, the nebulizer gas flow was 0.5 L min<sup>-1</sup>, and the integration time was 30 s.

A fully automated high-performance liquid chromatography (HPLC) system (TOSOH 8020, Tosoh, Tokyo, Japan) was used for the analysis of NTA, EDTA and DTPA. The HPLC system was composed of the following components: a DP-8020 pump, an AS-8021 auto sample injector, a CO-8020 column oven, a PD-8020 UV-VIS detector, PD-8020 data processing software, and TSK-gel ODS-80TM octadecylsilica columns (4.6 mm i.d. × 250 mm and 4.6 mm i.d. × 150 mm). The mobile phase solution consisted of 5 mM ammonium dihydrogenphosphate (pH 2.4) and was pumped at a flow rate of 0.5 mL min<sup>-1</sup> at 25°C. The injection volume was 20 μL, and detection was performed at 254 nm.

SPE was performed on a GL-SPE vacuum manifold kit (for 12 samples) (GL Sciences, Tokyo, Japan) combined with an air pump (CAS-1; AS ONE, Osaka, Japan). A Navi F-52 pH meter (Horiba Instruments, Kyoto, Japan) and a combination electrode were used for pH measurements.

A Barnstead 4-housing E-Pure water purification system (Barnstead/Thermolyne, Dubuque, IA, USA) was used to prepare deionized water, which is referred to as EPW hereafter.

## **2.2 Materials**

Analytical grade commercial products were used without further purification. Stock solutions (10 mM) of As(V), Cd(II), Cr(III), Pb(II) and Se(IV) were prepared from sodium arsenate heptahydrate (Na<sub>2</sub>HAsO<sub>4</sub>·7H<sub>2</sub>O; Kanto Chemical, Tokyo, Japan), cadmium (II) nitrate tetrahydrate (Cd(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O; Wako Pure Chemical, Osaka, Japan), chromium (III) nitrate nonahydrate (Cr(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O; Wako Pure Chemical, Osaka, Japan), lead (II) nitrate

( $\text{Pb}(\text{NO}_3)_2$ ; Wako Pure Chemical, Osaka, Japan) and sodium selenite ( $\text{NaSeO}_3$ ; Wako Pure Chemical, Osaka, Japan). Chelant stock solutions (10 mM) were prepared from nitrilotriacetic acid ( $(\text{HOOCCH}_2)_3\text{N}$ , NTA; Kanto Chemical, Tokyo, Japan), disodium dihydrogen ethylenediamine tetraacetate dihydrate ( $\text{C}_{10}\text{H}_{14}\text{N}_2\text{Na}_2\text{O}_8 \cdot 2\text{H}_2\text{O}$ , EDTA; Kanto Chemical, Tokyo, Japan) and diethylenetriamine-N,N,N',N'',N'''-pentaacetic acid ( $\text{C}_{14}\text{H}_{23}\text{N}_3\text{O}_{10}$ , DTPA; Dojindo Laboratories, Kumamoto, Japan). A multi-element solution (PlasmaCAL, SCP Science, Québec, Canada) containing 21 metals (Al, Ba, Be, Bi, Ca, Cd, Co, Cu, Fe, Ga, In, Mg, Mn, Ni, Pb, Sc, Sr, Ti, V, Y, and Zn) in 5%  $\text{HNO}_3$  was used to check the effects of diverse ions. Solutions of working standards ranging from  $\mu\text{M}$  to mM were prepared by dilution with EPW on a weight basis.

The experimental pH ranged from 4–9 and was adjusted using either 1 M HCl or 1 M NaOH. MES (2-(*N*-morpholino) ethanesulfonic acid monohydrate,  $\text{C}_6\text{H}_{13}\text{NO}_4\text{S} \cdot \text{H}_2\text{O}$ ; Sigma–Aldrich, St. Louis, MO, USA), HEPES (N-2-Hydroxyethylpiperazine-N'-2-ethanesulfonic acid,  $\text{C}_8\text{H}_{18}\text{N}_2\text{O}_4\text{S}$ ; Nacalai Tesque, Kyoto, Japan), and TAPS (N-Tris(hydroxymethyl)methyl-3-aminopropanesulfonic acid,  $\text{C}_7\text{H}_{17}\text{NO}_6\text{S}$ ; MP Biomedicals, Solon, OH, USA) were used as buffer reagents for pH 4–6, 7–8 and 9, respectively. Aqueous solutions of 10 mM chelating ligands in the appropriate buffer were spiked with 200  $\mu\text{M}$  of As(V), Cd(II), Cr(III), Pb(II) or Se(IV) to prepare the samples.

Different types of SPE materials were used, including an MRT gel, three chelating resins, and two ion exchange resins. The MRT gel type was AnaLig TE-01 (silica gel base containing crown ether functional groups; GL Sciences, Tokyo, Japan). The chelating resins were Chelex-100 (styrene divinylbenzene base containing iminodiacetic acid functional groups; Bio-Rad Laboratories, Hercules, CA, USA), NOBIAS Chelate PA-1 (hydrophilic methacrylate base containing polyamino-polycarboxylic acid functional groups; Hitachi High-Technologies, Tokyo, Japan), and NOBIAS Chelate PB-1 (divinylbenzene/

methacrylate polymer base containing polyamino-polycarboxylic acid functional groups; Hitachi High-Technologies, Tokyo, Japan). The ion exchange resins were NOBIAS Ion SA-1 (hydrophilic methacrylate base containing quaternized amine functional groups; Hitachi High-Technologies, Tokyo, Japan) and NOBIAS Ion SC-1 (hydrophilic methacrylate base containing sulfonic acid functional groups; Hitachi High-Technologies, Tokyo, Japan).

Low-density polyethylene bottles (Nalge Nunc, Rochester, NY, USA), perfluoroalkoxy (PFA) tubes and micropipette tips (Nichiryo, Tokyo, Japan) were used throughout the experiments. Before use, laboratory wares were first soaked in an alkaline detergent (Scat 20X-PF, Nacalai Tesque, Kyoto, Japan) overnight, and then in 4 M HCl overnight, followed by rinsing with EPW after each step.

Certified reference material (CRM) BCR-713 (effluent wastewater) from the European Commission Joint Research Centre, Institute of Reference Materials and Measurements (EC-JRC-IRMM), along with spiked soil washing solution (i.e., natural arsenic-contaminated soil from Hokkaido, Japan that was treated with 10 mM EDTA and spiked with a known amount of metal ions, followed by 6 h of shaking at room temperature) and spiked 'real' water samples (i.e., tap water from Kakuma, Kanazawa University, Kanazawa, Japan and water from Asano River, Kanazawa, Japan) were used for process validation. Cellulose membrane filters of 0.45  $\mu\text{m}$  pore size (Advantec, Tokyo, Japan) were used for the pre-separation step filtration treatment of the soil washing solution and the 'real' water samples.

### ***2.3 Experimental setup***

SPE materials were packed into 5 mL columns, and the columns were cleaned with 1 M  $\text{HNO}_3$  (8 mL) and EPW (6 mL). MES, HEPES or TAPS buffer solution (32~40 mL, 2 mL each loading) was allowed to flow through the column to ensure desired pH conditions from 4 to 9 in the SPE columns.

A total of 4 mL sample solution with pH already pre-adjusted with 0.1 M buffer solution (MES, HEPES or TAPS, whichever was appropriate) was passed through the SPE column at a controlled flow rate of  $0.2 \text{ mL min}^{-1}$ , and the column effluent was collected. The next step involved washing the column with EPW to remove the analyte fraction that was not retained. The final step was the elution of the ‘captured’ analyte with  $\text{HNO}_3$  (1 and 6 M) from the SPE system. The metal concentrations in the sample, column effluent, wash effluent and elution effluent were measured using the ICP-OES.

The terms extraction and recovery were used to explain the separation performance of the SPE systems and were calculated from the analyte concentrations in the column effluent, wash effluent and elution effluent. The extraction ratio (%) of each column for individual metal species was calculated by comparing the numbers of moles of analyte in the elution effluent with the cumulative number of moles of analyte present in all the effluents. The cumulative number of moles of analyte recovered from all fractions (i.e., column effluent, wash effluent and elution effluent) was compared with the numbers of moles of analyte in the solution that was loaded onto the column to calculate the recovery ratio (%).

Three replicates for each of the experiments were performed, and the average values were reported.

The workflow sequence for the separation of metal ions using SPE columns followed by ICP-OES determination is shown schematically in Fig. 1.

### **3.0 Results and discussion**

#### ***3.1 Comparative evaluation of MRT-SPE and other commercial SPE materials***

##### ***3.1.1 Extraction and recovery behavior***

Aqueous solutions containing toxic metal ions and APCs (NTA, EDTA and DTPA) in 1:50 molar ratios were treated with the MRT-SPE (AnaLig TE-01) and other commercial SPE materials (Chelex-100, NOBIAS Chelate PA-1, NOBIAS Chelate PB-1, NOBIAS Ion

SA-1, and NOBIAS Ion SC-1) to compare the separation efficiencies at optimized conditions. As shown in Fig. 2, when we evaluated the metal separation performance of the SPE columns with or without APCs, we concluded that excess chelant in solution resulted in considerable performance variations of the SPEs. It was also apparent that the MRT-SPE ensured quantitative extraction of the toxic metal ions from the aqueous solution with or without APCs. However, an exception should be noted for the aqueous systems containing NTA and Pb(II), which exhibited an extraction rate below 77% for all of the SPE systems. The MRT-SPE demonstrated superior extraction efficiency for EDTA-rich metal-fortified aqueous solutions when compared with other SPE systems, where the extraction rates were  $\leq 60\%$ . Separation of Cr(III) or Pb(II) from DTPA-rich aqueous solutions was quantitative for all the SPE systems, and aqueous systems with Pb(II) displayed similar behavior, even when no chelant was present in solution. The complete recovery of the metal ions that were ‘captured’ in the SPE columns was achieved with the MRT-SPE, while exceptions for As(V)- and Cr(II)-spiked solutions without chelant were observed for some of the commercial SPE materials other than MRT-SPE.

As(V) and Se(IV) have no known affinity for the APCs used here. However, those ions were simultaneously extracted with the APCs in solution, which subsequently reduced the extraction efficiencies of the SPEs (Fig. 2). These limitations were minimized with the use of MRT-SPE because the quantitative maximum extraction followed by recovery was achieved, compared with the other SPE systems.

### *3.1.2 Effect of the metal-chelant stability constant*

APCs (i.e., NTA, EDTA or DTPA) form water-soluble metal complexes of high thermodynamic stability (Lim et al., 2005) of varying metal-chelant stability constants ( $K_{ML}$ ) with Cd(II), Cr(III) or Pb(II) (Table 1), which may influence the separation performance of the SPE materials. The effect of the metal-chelant complexes’ conditional stability constants

( $K'_{ML}$ , at pH 7) on the performance of MRT-SPE and other commercial SPE materials was studied for the extraction of Cd(II), Cr(III) or Pb(II) ions from chelant-rich, metal-spiked aqueous system (Fig. 3). AnaLig TE-01 demonstrated better effectiveness than the other SPE materials (i.e., Chelex-100, NOBIAS Chelate PA-1, NOBIAS Chelate PB-1, NOBIAS Ion SA-1, NOBIAS Ion SC-1) for Cd(II), Cr(III) or Pb(II) separation from EDTA-rich aqueous solutions. Comparable separation performances for Cd(II) or Pb(II) were observed for excess DTPA-containing solutions.

The Pb(II) extraction rate with MRT-SPE from NTA-rich mixtures was only  $57.5 \pm 1.9\%$ , but none of the SPE columns were capable of ensuring its quantitative extraction. It is likely that the separation between metals and chelants (i.e., the extraction of metal) will be easier when the stability constant of the metal-chelant complex is low. The  $K'_{ML}$  (at pH 7) of the Pb(II)-NTA complex (8.82) in the aqueous matrix was lower than that for EDTA and DTPA, and the quantitative maximum Pb(II) extraction rate was expected from NTA-containing solutions as it was obtained for EDTA and DTPA. However, Pb(II) oxide has a propensity to precipitate at neutral pH. Such precipitation is facilitated as a result of the lower affinity between NTA and Pb, which has a significant effect on the extraction capacity of the SPE system. Although the  $K'_{ML}$  of Cd(II)-NTA complex (7.10) was also comparatively low, Cd(II) ions remain soluble in the aqueous matrix at pH 7 and have no such effect on the extraction performance.

In general, we note that MRT-SPE can effectively be used to separate metal ions from the chelant-rich aqueous solutions for metal-chelant stability constants up to 18.8, which is the  $K_{ML}$  value for Pb(II)-DTPA, with exception of the behavior of Pb(II) with NTA. The MRT-SPE appeared as the solitary potential option for the separation of toxic metal ions from aqueous solutions containing an excess of EDTA, which is the most widely used APC for metal-contaminated waste treatment.

### ***3.2 Effect of variables on the performance of MRT-SPE***

#### ***3.2.1 pH***

The separation performance of the AnaLig TE-01 SPE column was studied as a function of pH and was described in terms of extraction and recovery rate (Fig. 4). The experimental conditions utilized EDTA, considering its frequent use among the APCs. Therefore, the study was restricted to the pH range from 4–9 because of the insufficient solubility of EDTA at very low pH in aqueous media (Ueno et al., 1992). The increasing solubility of silica gel with increasing pH (Vogelsberger et al., 1992), which may dissolve the silica gel base support of AnaLig TE-01 column, was also a concern. Nearly similar extraction patterns for As(V) or Se(IV) were observed with or without EDTA in solution, which established that the excess chelant in the aqueous system had no significant influence on the solubility or separation aptitude of those metals. However, a significant drop in the extraction rate of As(V) or Se(IV) above a pH of 8 was observed, which may have been due to increased concentrations of the competitive ions ( $\text{OH}^-$  or  $\text{HL}^{3-}$ ) in the system. An extraction rate of  $\geq 98\%$  for Cd(II), Cr(III) and Pb(II) from pH 5 to 7 was attained from metal-fortified solutions containing an excess of chelant, while the changes in the recovery rates were insignificant in terms of pH. The decrease in the extraction rate at  $\text{pH} < 5$  or  $> 7$  can be attributed either to an excess of  $\text{H}^+$  ions in the acidic region or  $\text{OH}^- / \text{HL}^{3-}$  ions in the basic region, respectively. Subsequent experiments with the MRT-SPE column were conducted at pH 7 to minimize any possible effects from the competitive ions.

#### ***3.2.2 Sample loading flow rate***

The loading flow rates of metal-fortified sample solutions have a significant influence on metal retention rates in SPE columns (Bag et al., 1998). The effects of sample loading flow rates were studied in the range of  $0.2\text{--}5 \text{ mL min}^{-1}$ . A gradual decrease in retention capacities of the MRT-SPE column was observed with increasing flow rates above  $0.25 \text{ mL min}^{-1}$  (Fig.

5). A constant retaining capability of the MRT-SPE column at the initial loading period is indicated by such behavior; therefore, a flow rate of  $0.2 \text{ mL min}^{-1}$  was applied for subsequent experiments.

### 3.2.3 Eluent

Eluent selected for a particular separation process should be capable of extracting the analyte, thereby facilitating its quantitative determination (Chen et al., 2009). Analytes retained in the MRT-SPE column were eluted with  $\text{HNO}_3$  (4 mL) of varying concentrations (0.1–6 M), which all displayed constant recovery rates for eluent concentrations above 0.5 M (Fig. 6). However, IBC Advanced Technologies (2007) recommended the use of  $\geq 5 \text{ M}$  acids for the elution of bound ions in the TE-01 SPE column. Hence, a combination of 1 M  $\text{HNO}_3$  (2 mL) and 6 M  $\text{HNO}_3$  (1 mL) was selected as the eluent for subsequent experiments to ensure the complete elution of the analyte when treated with TE-01.

### 3.3 Effect of diverse metal ions

The interference caused by complexing species results in significant problems towards the quantitative extraction of analytes (Prabhakaran and Subramanian, 2003). To examine the separation efficiency of MRT-SPE in the presence of various interfering metal ions, studies were performed using PlasmaCAL multi-element metal ion solutions spiked with the target metal ions and APCs. EDTA was used as the representative APC because EDTA has most often been utilized among the APCs, owing to its capacity to form water-soluble chelant complexes with most toxic metals (Egli, 2001; Nowack and VanBriesen, 2005; Leštan et al., 2008). The metal-to-chelant ratio was maintained at 1:50, and the final solutions were allowed to equilibrate for 24 h before analysis. The extraction and recovery rates demonstrated the superior ion selective separation performance of the MRT-SPE in the presence of large concentrations of matrix components (Table 2).

### ***3.4 Retention capacity of the MRT-SPE***

The stability of the SPE system during the separation process can be determined from its retention capacity, which is calculated from the breakthrough volume (i.e., the volume of sample that causes the target analyte to be eluted from the SPE material) and the analyte concentration (Yu et al., 2003). Metal-spiked sample solutions were passed through the MRT-SPE column, eluted and subjected to ICP-OES analysis to estimate the retention capacity expressed in terms of mmol of analyte captured in one gram of SPE material. The retention capacities of the MRT-SPE ( $\text{mmol g}^{-1}$ ) at pH 7 were as follows:  $0.44 \pm 0.04$  for As(V),  $0.41 \pm 0.06$  for Cd(II),  $0.05 \pm 0.02$  for Cr(III),  $0.48 \pm 0.06$  for Pb(II), and  $0.34 \pm 0.05$  for Se(IV). The matrix was  $\text{H}_2\text{O}$ , the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution consisted of 2 mL of 1 M  $\text{HNO}_3$ , 1 mL of 6 M  $\text{HNO}_3$ , and 1 mL of EPW.

### ***3.5 Regeneration ability of the MRT-SPE***

The regeneration ability of the MRT-SPE was investigated with sample solutions spiked with  $200 \mu\text{M}$  of As(V) or Pb(II) ions and 10 mM of EDTA in aqueous matrix. Again, the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution contained 2 mL of 1 M  $\text{HNO}_3$ , 1 mL of 6 M  $\text{HNO}_3$ , and 1 mL of EPW. The extraction rates of the fresh column (As(V):  $99.0 \pm 0.1$ ; Pb(II):  $100 \pm 0.1$ ) and after 100 cycles (As(V):  $97.2 \pm 4.1$ ; Pb(II):  $98.4 \pm 0.3$ ) were evaluated to conclude that more than 100 loading and elution cycles could be performed using MRT-SPE without any loss of analytical performance.

### ***3.6 Accuracy and applications***

#### ***3.6.1 Recovery of metals from certified reference material***

EC-JRC-IRMM CRM, namely BCR-713 (effluent wastewater), spiked with  $10 \mu\text{M}$  of EDTA (pH maintained at 7 with HEPES buffer), was used to evaluate the accuracy of the proposed separation process (Table 3). The recovery rates for As(V) and Cd(II) were 89.7 and 101.4%, respectively, while Cr(III), Pb(II) or Se(IV) were not detected.

### 3.6.2 Recovery of metals from 'real' water samples and soil washing effluent

The proposed separation process was applied to the analysis of local natural water samples (i.e., both tap water and river water) and soil washing effluent. The samples were spiked with known amounts of As(V), Cd(II), Cr(III), Pb(II) or Se(IV) and 10 mM of EDTA, followed by MRT-SPE separation and ICP-OES analysis (Table 4). Recoveries at varying rates (99–101% for As(V), 84–102% for Cd(II), 101–102% for Cr(III), 98–100% for Pb(II), and 88–100% for Se(IV)) from metal-spiked excess chelant-containing solutions were observed.

## 4.0 Conclusion

The recoveries of As(V), Cd(II), Cr(III), Pb(II) and Se(IV) from simulated washing effluents containing an excess of APCs (i.e., NTA, EDTA or DTPA) was accomplished with an ion-selective immobilized macrocyclic material, commonly known as MRT gel. The MRT-SPE system showed optimum separation performance in the pH range of 5 to 7. Quantitative extraction occurred using a sample loading flow rate of  $0.2 \text{ mL min}^{-1}$ , and the 'captured' metal ions were eluted with a mixture of 1 and 6 M  $\text{HNO}_3$ . The MRT-SPE was stable during operation and enabled more than 100 loading and elution cycles to be performed without any loss of analytical performance. The non-destructive treatment of chelant-enriched metal-contaminated effluent with the subsequent option to recycle the processed water and metal ions are the major focal points of the proposed separation process.

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Table 1: Acid dissociation constants ( $pK_a$ ), stability constants ( $K_{ML}$ ) and conditional stability constants ( $K'_{ML}$ ) of metal-ligand complexes at 25°C ( $\mu = 0.1$ )<sup>a</sup>.

APCs	$pK_a$					$K_{ML}$			$K'_{ML}$ (at pH 7)		
	$pK_{a1}$	$pK_{a2}$	$pK_{a3}$	$pK_{a4}$	$pK_{a5}$	$Cd^{2+}$	$Cr^{3+}$	$Pb^{2+}$	$Cd^{2+}$	$Cr^{3+}$	$Pb^{2+}$
NTA	1.81	2.52	9.66			9.76	NA <sup>b</sup>	11.48	7.10	-	8.82
EDTA	2.00	2.69	6.13	10.19		16.5	23.4	18.0	13.3	20.2	14.8
DTPA	2.0	2.70	4.28	8.60	10.50	19.0	NA <sup>b</sup>	18.8	15.5	-	15.3

<sup>a</sup> Martell et al. (2004).

<sup>b</sup> NA = Not available. Data not available in the critically selected NIST database

Table 2. Separation performance of the MRT-SPE column in the presence of various interfering metal species in the matrix<sup>a</sup>.

Species	Extraction (%)	Recovery (%)
As(V)	99.6±3.4	100±4.2
Cd(II)	101±4.7	100±1.6
Cr(III)	98.7±3.9	99.4±1.1
Pb(II)	100±2.5	97.8±3.4
Se(IV)	97.7±3.6	102±2.1

<sup>a</sup> Sample solutions were composed of 200 μM As(V), Cd(II), Cr(III), Pb(II), or Se(IV). The chelant was 10 mM EDTA, and the matrix was H<sub>2</sub>O. The matrix ions included Al, Ba, Be, Bi, Ca, Cd, Co, Cu, Fe, Ga, In, Mg, Mn, Ni, Pb, Sc, Sr, Ti, V, Y, and Zn. The solution pH was 7, the sample volume was 4 mL, the flow rate was 0.2 mL min<sup>-1</sup>, and the elution solution consisted of 1 M HNO<sub>3</sub> (2 mL) + 6 M HNO<sub>3</sub> (1 mL) + EPW (1 mL) (*n* = 3).

Table 3. Separation of metals from certified reference material BCR-713 (effluent wastewater).

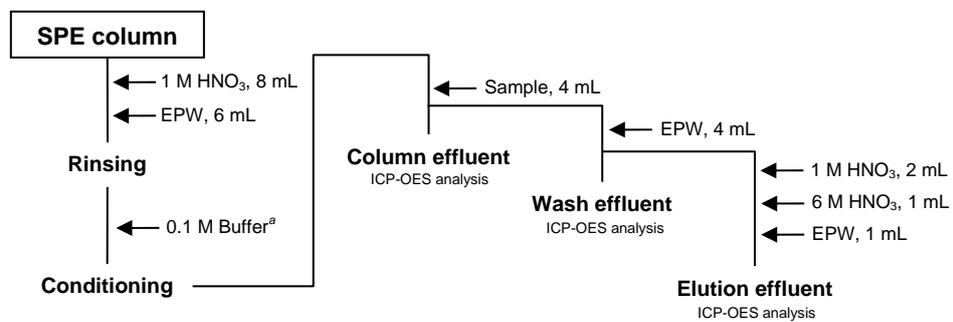
<i>Certified data</i> <sup>a</sup>		<i>This work</i>	
Species	Value ( $\mu\text{g L}^{-1}$ )	Species	Value ( $\mu\text{g L}^{-1}$ )
As	9.7±1.1	As(V)	8.7±0.8
Cd	5.1±0.6	Cd(II)	5.2±0.7
Cr	21.9±2.4	Cr(III)	ND <sup>b</sup>
Pb	47±4	Pb(II)	ND <sup>b</sup>
Se	5.6±1.0	Se(IV)	ND <sup>b</sup>

<sup>a</sup> Certified by EC-JRC-IRMM (European Commission Joint Research Centre, Institute of Reference Materials and Measurements)

<sup>b</sup> ND = Not detected.

Table 4. Separation of metals from spiked samples of 'real' waters and soil washing effluent.

<i>Sample</i>		<i>As(V)</i>	<i>Cd(II)</i>	<i>Cr(III)</i>	<i>Pb(II)</i>	<i>Se(IV)</i>
	Added ( $\mu\text{g L}^{-1}$ )	15.0	22.5	10.4	41.4	15.8
<i>Tap Water</i>	Found ( $\mu\text{g L}^{-1}$ )	14.9 $\pm$ 0.3	18.9 $\pm$ 0.9	10.5 $\pm$ 1.5	40.8 $\pm$ 3.1	15.9 $\pm$ 1.2
	Recovery (%)	99.4	83.9	101.1	98.3	100.4
<i>River Water</i>	Found ( $\mu\text{g L}^{-1}$ )	15.1 $\pm$ 0.5	22.8 $\pm$ 0.7	10.6 $\pm$ 0.2	41.6 $\pm$ 0.8	15.8 $\pm$ 0.3
	Recovery (%)	100.6	101.5	101.9	100.3	100.0
<i>Soil washing effluent</i>	Found ( $\mu\text{g L}^{-1}$ )	15.0 $\pm$ 0.3	22.5 $\pm$ 0.9	10.6 $\pm$ 0.5	41.5 $\pm$ 0.9	13.8 $\pm$ 1.4
	Recovery (%)	100.3	100.3	101.5	100.2	87.5



<sup>a</sup> 32–40 mL, MES buffer (pH 4–6), HEPES buffer (pH 7–8), TAPS buffer (pH 9)

Fig. 1: Schematic workflow diagram of the separation process

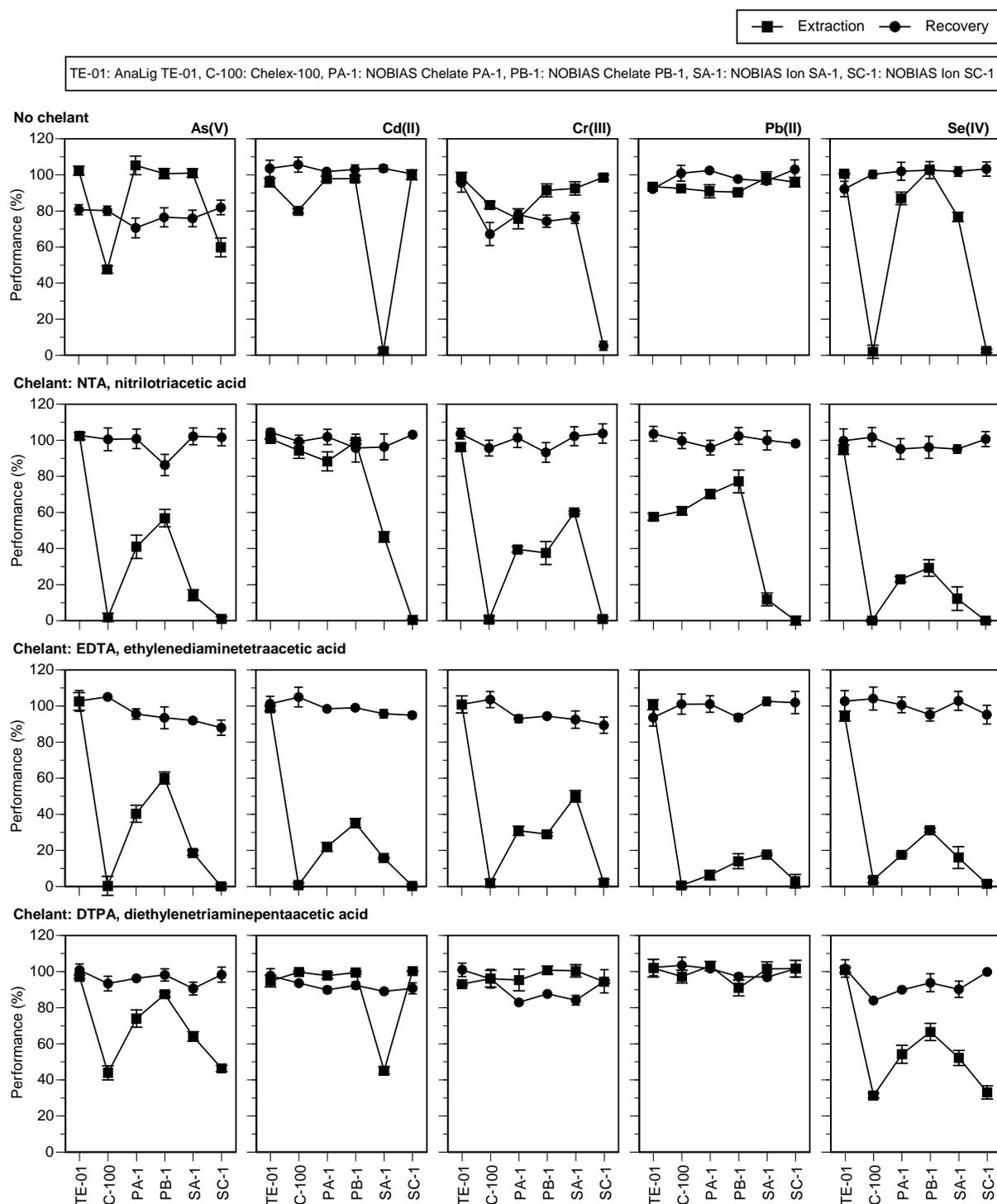


Fig. 2: Comparative performance of different SPE columns. The sample solutions were composed of 200  $\mu\text{M}$  As(V), Cd(II), Cr(III), Pb(II), or Se(IV). The chelant was 10 mM NTA, EDTA, DTPA or EDDS and the matrix was  $\text{H}_2\text{O}$ . The solution pH was 7, the sample volume was 4 mL, the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution consisted of 1 M  $\text{HNO}_3$  (2 mL) + 6 M  $\text{HNO}_3$  (1 mL) + EPW (1 mL) ( $n = 3$ ).

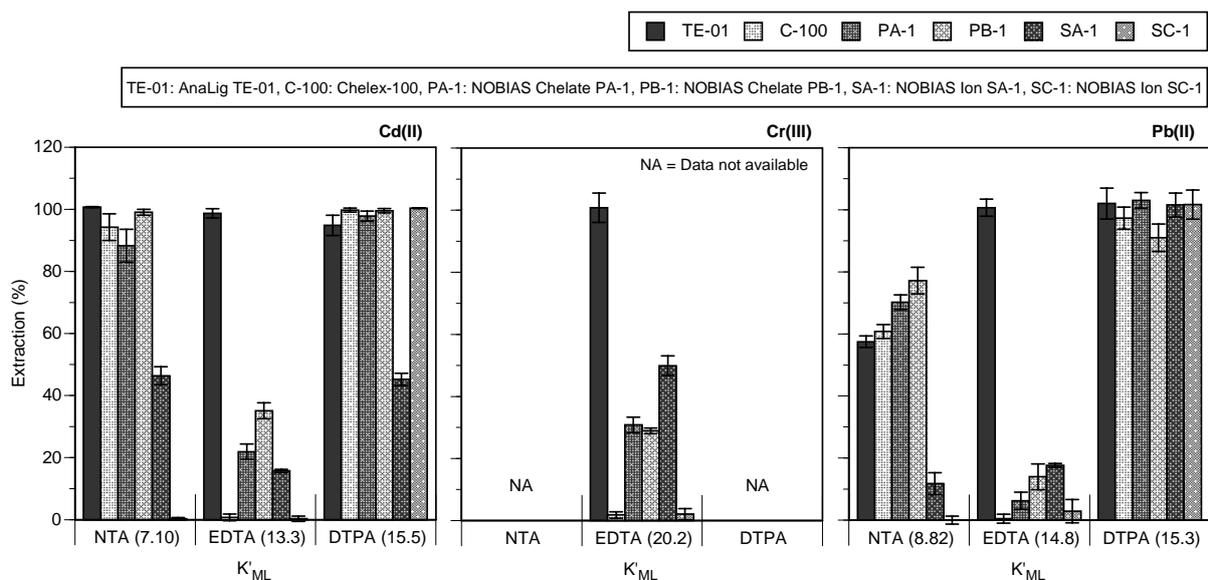


Fig. 3: Effect of metal-chelant stability constants on the performance of SPE materials. The sample solutions were composed of 200  $\mu\text{M}$  Cd(II), Cr(III) or Pb(II), and the chelant was 10 mM NTA, EDTA or DTPA. The matrix was  $\text{H}_2\text{O}$ , the solution pH was 7, the sample volume was 4 mL, the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution consisted of 1 M  $\text{HNO}_3$  (2 mL) + 6 M  $\text{HNO}_3$  (1 mL) + EPW (1 mL) ( $n = 3$ ).

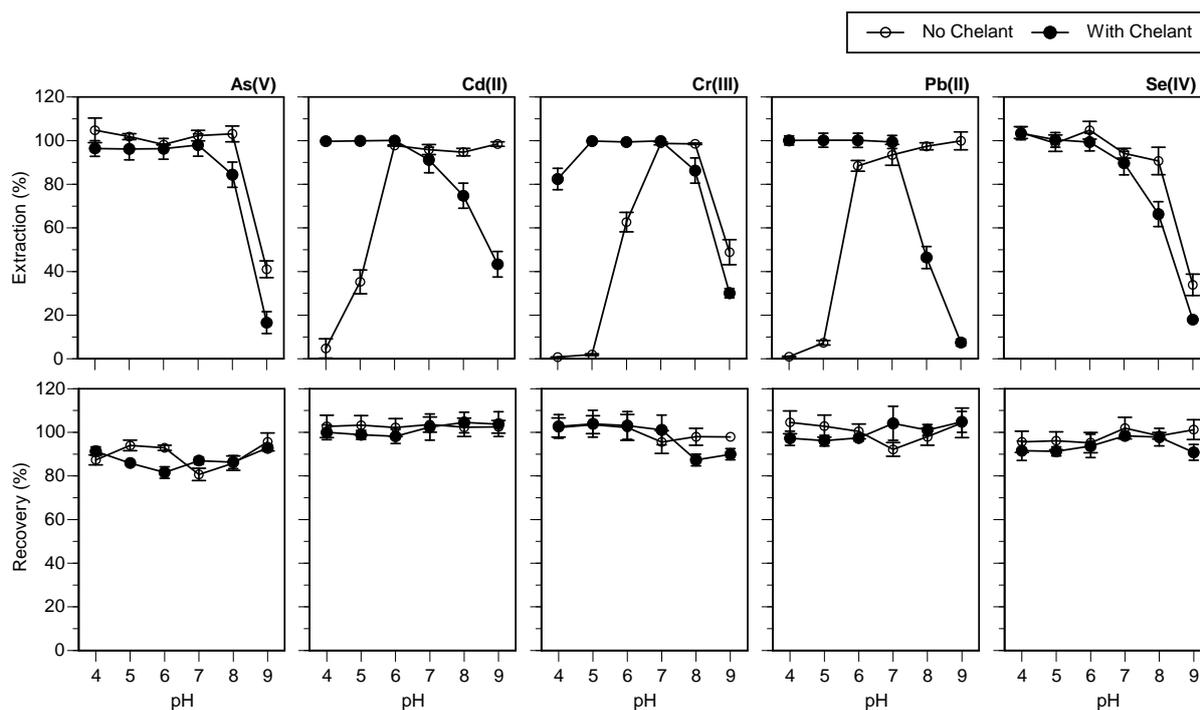


Fig. 4: Extraction and recovery performance of the MRT-SPE column as a function of pH, with or without chelant. The sample solutions were composed of 200  $\mu\text{M}$  As(V), Cd(II), Cr(III), Pb(II), or Se(IV). The chelant was 10 mM EDTA, and the matrix was  $\text{H}_2\text{O}$ . The pH ranged from 4 to 9, the sample volume was 4 mL, the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution consisted of 1 M  $\text{HNO}_3$  (2 mL) + 6 M  $\text{HNO}_3$  (1 mL) + EPW (1 mL) ( $n = 3$ ).

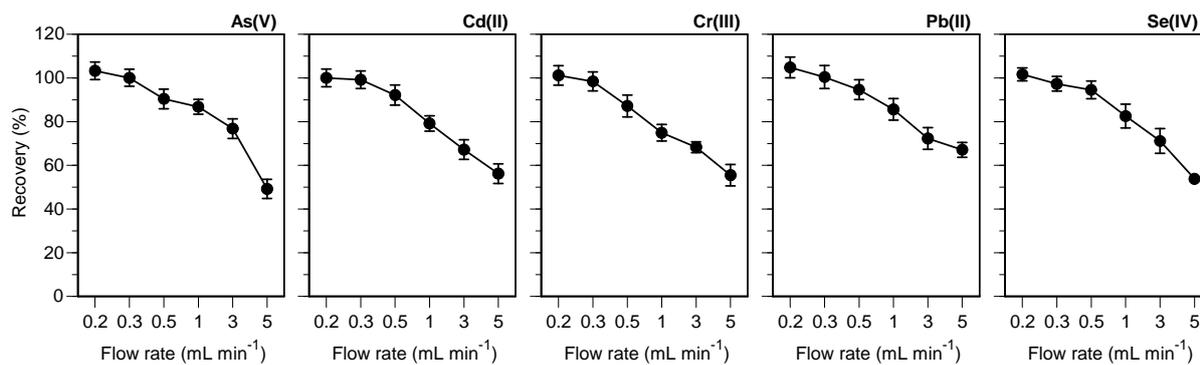


Fig. 5: Effect of sample loading flow rates on the separation performance of the MRT-SPE column. The sample solutions were composed of 200  $\mu\text{M}$  As(V), Cd(II), Cr(III), Pb(II), or Se(IV). The chelant was 10 mM EDTA, and the matrix was  $\text{H}_2\text{O}$ . The pH was 7, the sample volume was 4 mL, the flow rate ranged from 0.2–5  $\text{mL min}^{-1}$ , and the elution solution consisted of 1 M  $\text{HNO}_3$  (2 mL) + 6 M  $\text{HNO}_3$  (1 mL) + EPW (1 mL) ( $n = 3$ ).

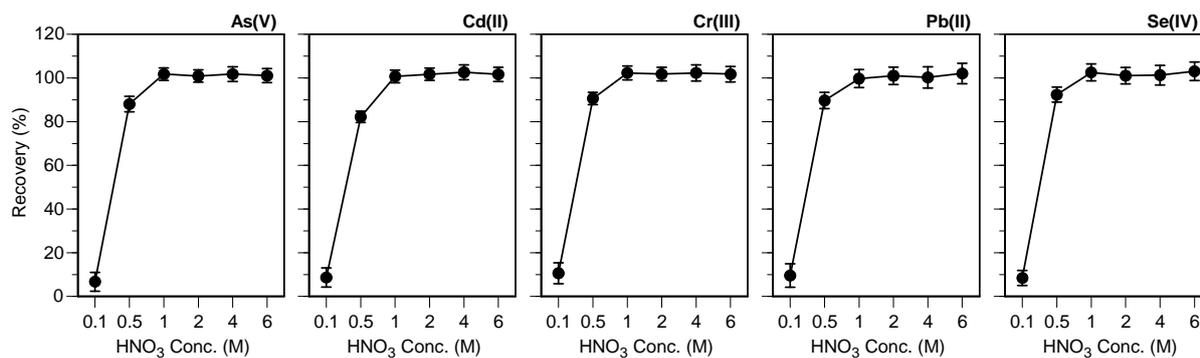


Fig. 6: Effect of eluent concentration on the separation performance of the MRT-SPE column. The sample solutions were composed of 200  $\mu\text{M}$  As(V), Cd(II), Cr(III), Pb(II), or Se(IV). The chelant was 10 mM EDTA, and the matrix was  $\text{H}_2\text{O}$ . The solution pH was 7, the sample volume was 4 mL, the flow rate was  $0.2 \text{ mL min}^{-1}$ , and the elution solution consisted of 0.1–6 M  $\text{HNO}_3$  (3 mL) + EPW (1 mL) ( $n = 3$ ).